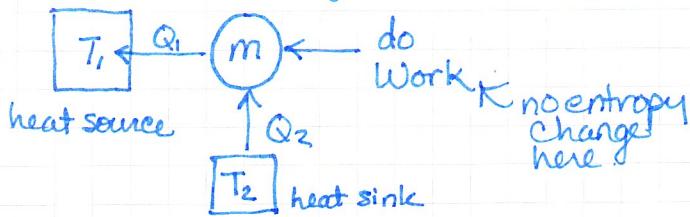


Lecture 9 Refrigeration Cycles

(A) If you run a heat engine in reverse, you get a refrigeration process



$$1^{\text{st}} \text{ Law: } Q_2 + W = Q_1$$

$$2^{\text{nd}} \text{ Law: } \Delta S_{\text{tot}} \geq 0 \quad \Delta S = \frac{Q_1}{T_1} - \frac{Q_2}{T_2} \geq 0 \quad \frac{Q_1}{T_1} \geq \frac{Q_2}{T_2} \quad \frac{Q_1}{Q_2} \geq \frac{T_1}{T_2}$$

(B) What is the performance of a refrigerator?

$$\text{Coefficient of performance } \eta_{\text{Ref}} = \frac{Q_2}{W} = \frac{Q_2}{Q_1 - Q_2}$$

$$\frac{1}{\eta_{\text{Ref}}} = \frac{Q_1 - Q_2}{Q_2} = \frac{Q_1}{Q_2} - 1 \quad \frac{1}{\eta_{\text{Ref}}} \geq \frac{T_1}{T_2} - 1 = \frac{T_1 - T_2}{T_2}$$

A reversible cycle takes an infinite amount of time

$$\text{Example: } \eta_{\text{Ref}}^{\max} = \frac{T_2}{T_1 - T_2} = \frac{273K}{27K} = 10$$

In an ideal refrigerator, for every 1KW of electricity you get 6 KW of heat.

(C) Inverse of this cycle is a heat pump.
It heats the reservoir

$$\eta_{\text{HP}} = \frac{Q}{W} = \frac{Q_1}{Q_1 - Q_2} \quad \frac{1}{\eta_{\text{HP}}} = \frac{Q_1 - Q_2}{Q_1} = 1 - \frac{Q_2}{Q_1} \geq 1 - \frac{T_2}{T_1}$$

Same cycle - want to get as much Q for input W

$$\eta_{\text{HP}} \leq \frac{T_1}{T_1 - T_2} \quad \text{example: OAT} = 273K \quad \text{maximum coef of hp performance} \quad \eta_{\text{HP}}^{\max} = \frac{298}{25} \approx 12$$

consider mechanism M as a frictionless piston

$$\eta_{\text{HP}}^{\max} = \frac{T_1 - T_2}{T_1} =$$

for a perfect gas temperature scale $PV = R \Theta$ got from triple point

So that is how to prove that the temperature scale is the absolute temperature scale

Phase Equilibria

Mixing of entropies

$$S = S_1 + S_2 = S_1(E_1, V_1, N_1) + S_2(E_2, V_2, N_2)$$

$$\boxed{\begin{matrix} E_1 V_2 \\ N_2 \end{matrix}}$$

$$\boxed{E, V, N, 1}$$

now, not applying statistical mechanics - only classical thermodynamics.

System is isolated in some thermal insulating container

$$E_1 + E_2 = E_0 \quad V_1 + V_2 = V_0 \quad N_1 + N_2 = N_0$$

Note:
N is NOT
avagadro's
number

$$\therefore S(E_1, V_1, N_1) = S_1(E_1, V_1, N_1) + S_2(E_2, V_2, N_2), \text{ can be expressed}$$

in terms of system
parameters

$$\frac{\partial S}{\partial E_1} = 0 \Rightarrow \frac{\partial S_1}{\partial E_1} + \frac{\partial S_2}{\partial E_2} = 0 \Rightarrow \frac{\partial S_1}{\partial E_1} + \frac{\partial S_2}{\partial E_2} \frac{\partial E_2}{\partial E_1} = 0 \Rightarrow \frac{\partial S_1}{\partial E_1} - \frac{\partial S_2}{\partial E_2} = 0$$

$$\therefore \frac{\partial S_1}{\partial E_1} = \frac{\partial S_2}{\partial E_2} \Rightarrow \frac{1}{T_1} = \frac{1}{T_2}$$

$$\frac{\partial S}{\partial V_1} = 0 \Rightarrow \frac{\partial S}{\partial V_1} + \frac{\partial S_2}{\partial V_2} = 0 \Rightarrow \text{use } \frac{\partial S_2}{\partial V_2} = \frac{\partial S_2}{\partial V_1} \frac{\partial V_2}{\partial V_1} = -\frac{\partial S_2}{\partial V_2} \quad \frac{\partial V_2}{\partial V_1} = -1$$

$$\text{we had } \left(\frac{\partial S}{\partial V}\right)_{E,V} = \frac{P}{T} \quad \text{this equation leads to } \frac{P_1}{T_1} = \frac{P_2}{T_2}$$

\therefore the pressures $P_1 = P_2$ of the two phases must be the same.

Find maximum entropy

$$\frac{\partial S}{\partial N_1} = 0 \quad \frac{\partial S_1}{\partial N_1} + \frac{\partial S_2}{\partial N_2} \frac{\partial N_2}{\partial N_1} = 0 \Rightarrow \frac{\partial S}{\partial N_1} = \frac{\partial S}{\partial N_2} \quad \text{keep energy + volume fixed}$$

$$\left(\frac{\partial S}{\partial N}\right)_{E,V} = \frac{\mu}{T} \quad \text{chemical potential}$$

$$-\frac{\mu_1}{T_1} = -\frac{\mu_2}{T_2} \quad \therefore \mu_1 = \mu_2 \quad \text{new condition of equilibrium}$$

$$\boxed{\mu = -T \left(\frac{\partial S}{\partial N}\right)_{E,V}}$$

chemical potential

$T, P = \text{constant}$ look at system another way. G is a minimum

$$G = G_1 + G_2 \quad \text{Gibb's free energy of the two phases.}$$

Lecture 9 continued...

Fundamental Thermodynamic Energy

previously: $dE = TdS - PdV$ when $N = \text{constant}$

$$S \equiv S(E, V, N)$$

$$dS = \left(\frac{\partial S}{\partial E}\right)_{V,N} dE + \left(\frac{\partial S}{\partial V}\right)_{E,N} dV + \left(\frac{\partial S}{\partial N}\right)_{E,V} dN$$

$$dS = \frac{1}{T} dE + \frac{P}{T} dV - \frac{\mu}{T} dN$$

$$\boxed{TdS = dE + PdV - \mu dN}$$

Gibb's Free Energy

$$G \equiv G(P, T, N)$$

$$dG = \left(\frac{\partial G}{\partial P}\right)_{T,N} dP + \left(\frac{\partial G}{\partial T}\right)_{P,N} dT + \left(\frac{\partial G}{\partial N}\right)_{P,T} dN$$

$$\boxed{dG = VdP - SdT + \mu dN}$$

$$\left(\frac{\partial G}{\partial N}\right)_{P,T} = \mu$$

$$G = \mu N + \chi(P, T)$$

^ integration constants

$$\lim_{N \rightarrow 0} G = 0 = \chi(P, T) \therefore \chi(P, T) = 0$$

$$G = \mu N$$

$$\mu = \frac{G}{N} = g \quad \text{Gibb's free energy per unit molecule}$$

$$\mu = g(T, P) \quad \text{recall } T, P \text{ are intensive variables}$$

not extensive variables

$$G = N_1 g_1 + N_2 g_2$$

at equilibrium G is a minimum

$$dG = 0 \quad \begin{matrix} @ \text{minimum} \\ @ \text{equilibrium} \end{matrix}$$

$$dG = g_1(T, P) dN_1 + g_2(T, P) dN_2 = 0$$

$$N_1 + N_2 = N_0 \rightarrow dN_1 = -dN_2$$

$$dG = [g_1(T, P) - g_2(T, P)] dN_1 = 0$$

since this has to be zero for any dN_1 ,

$$g_1(T, P) = g_2(T, P)$$

$$G = N_1 g_1 + N_2 g_2$$

If $g_1 < g_2$ then all particles will go to $N_1 = N$ $N_2 = 0$

all particles go into phase 1

If $g_2 < g_1$ then to minimize G everything should go into phase 2, $N_1 = 0$ $N_2 = N$

The important point is that they will always coexist.

